



**All-Russian Scientific Research  
Institute of Refrigeration Industry -  
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Academy of Science**

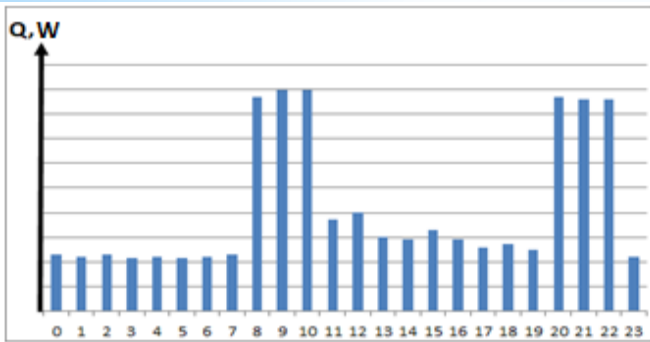
- \* **Investigation of heat and mass transfer processes during film flow around ice surfaces with a phase transition to create a new generation of ice banks**

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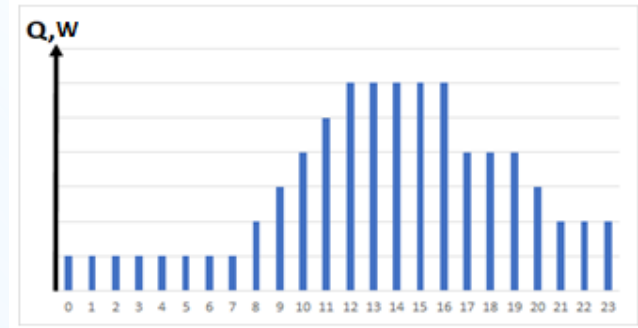
Speaker: Borschev G.V.

# 1.Relevance

Cooling of food processing facilities with a high degree of uneven heat load distribution



Typical daily distribution of heat load at a grassroots dairy enterprise



Typical daily distribution of heat load at an industrial dairy enterprise



REFRIGERATION

Cooling without ice bank

Benefits of ice bank

- 1.High equipment cost
- 2.High electricity price during daytime operation
3. The total refrigerating capacity of the refrigeration units should be equal to  $Q_{max}$  - the maximum heat load



- 1.Reduction of capital costs for refrigeration equipment
- 2.Reducing energy costs when using the night rate
3. The total refrigerating capacity of the refrigeration park is significantly lower than  $Q_{max}$  - the maximum heat load

## 2. Purpose of Research

Studying the processes of heat and mass transfer during film flow around ice structures with a phase transition to create heat exchangers of a new generation with a high efficiency of heat removal, coupled with the graph of the current heat load is the purpose of research.



Water ice

$$t_{\text{melt}} = 0^{\circ}\text{C}$$

non-toxic

$$\lambda = 335 \frac{\text{kJ}}{\text{kg}}$$

The main disadvantage of this type of ice banks is the low heat transfer coefficient when ice is melted in a large volume

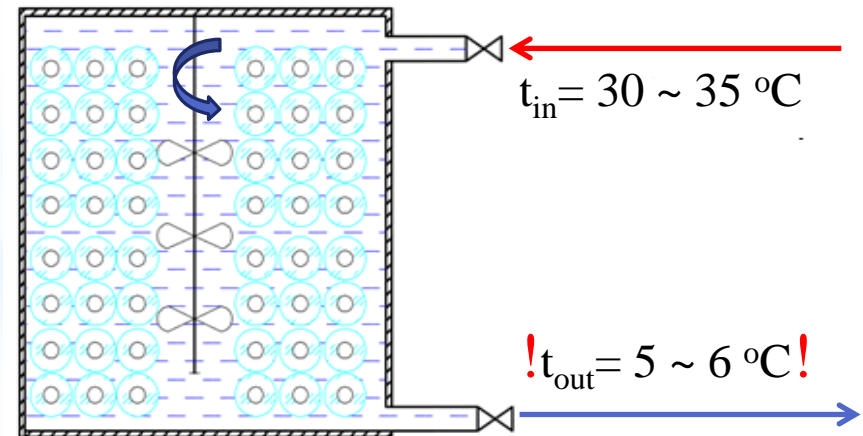
$$\alpha = 300 \sim 500 \text{ W}/(\text{m}^2 \cdot ^{\circ}\text{C}) \longrightarrow \uparrow t_{\text{out}}$$

Problems to be solved:

- development of an experimental stand
- development of research methods
- experimental research
- determination of the influence of the flow rate and temperature of the supplied water on the efficiency of heat and mass transfer
- processing of experimental data and analysis of the results.



Volumetric melting ice bank



Volumetric ice bank discharge process

### 3. Advantages of film melting

Film flow without phase transition

Application: Spray - type heat exchangers

Feature: High efficiency of heat transfer

Existing dependencies:

$$\alpha = a \frac{\Gamma^{0,257}}{H^{0,05}} (1 + bt) \text{ (Ploeg)}$$

$$\alpha = 40 \frac{\Gamma^{0,4}}{d^{0,6}} \text{ (Adams)}$$

$$\alpha = 122l^{0,4} \text{ (Semilet)}$$

$$\alpha > 5000 \text{ W}/(\text{m}^2 \cdot \text{°C})$$

Volumetric melting

Application: Volumetric melting ice banks

Feature: Phase transition of ice in the volume of liquid

$$\downarrow \alpha = 300 \sim 500 \text{ W}/(\text{m}^2 \cdot \text{°C})$$

Film flow around melting surfaces

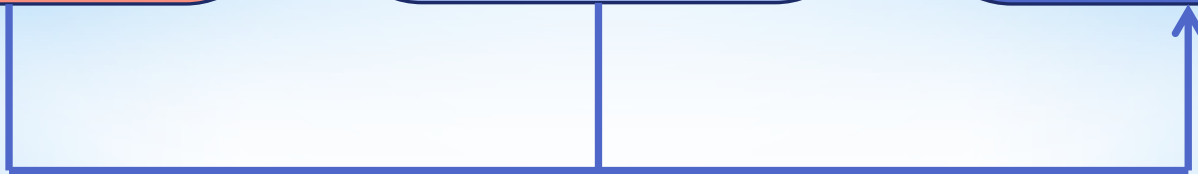
Application: Film Ice banks

Feature: High efficiency of heat exchange + phase transition of ice

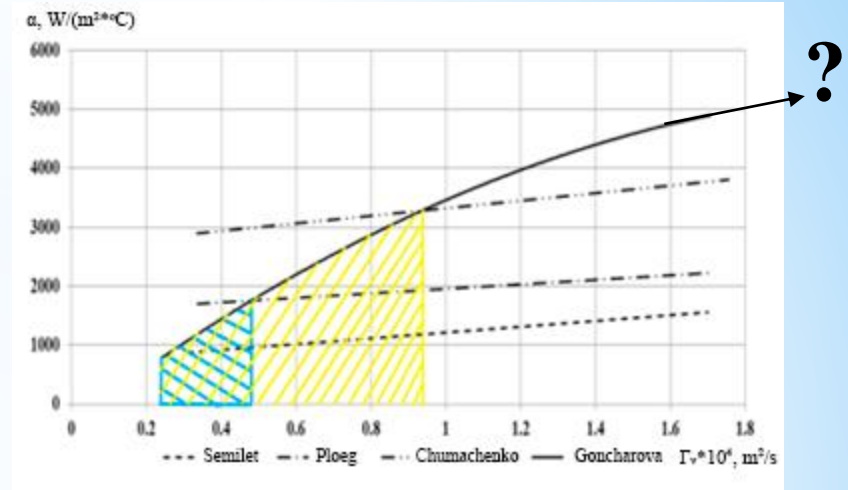
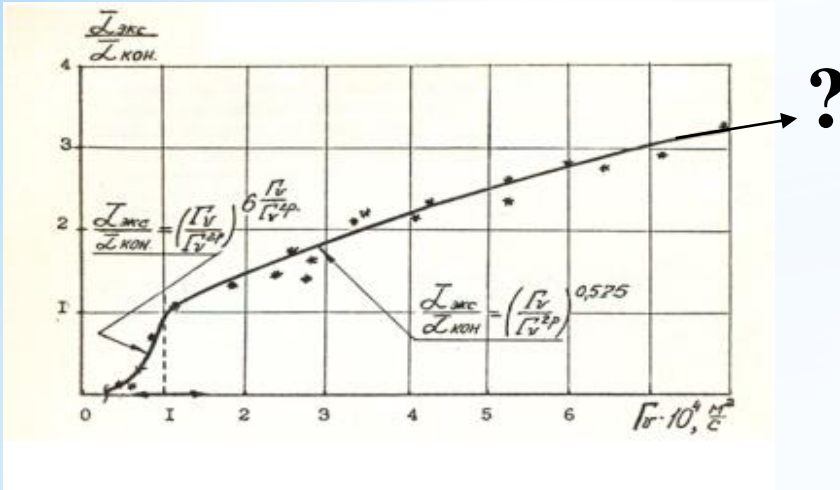
Existing dependencies : ?



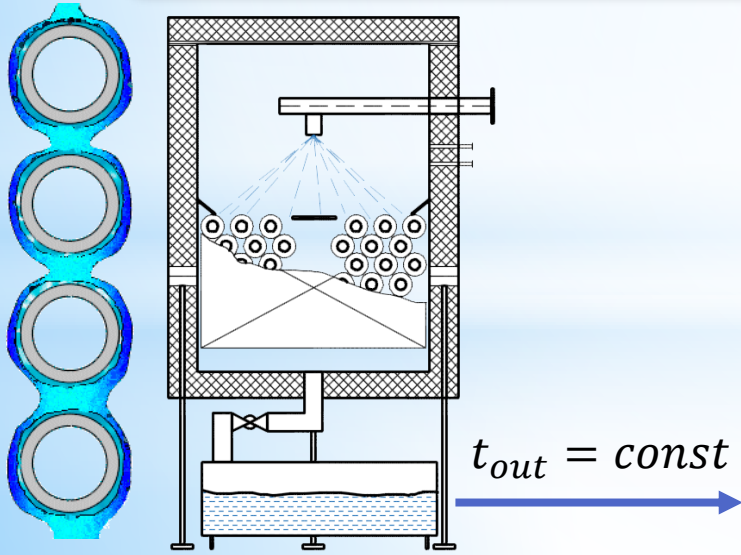
$$\uparrow \alpha = 7000 \text{ W}/(\text{m}^2 \cdot \text{°C})$$



# 4. Results of the literature review



Data obtained in the study of horizontally separated flow around coaxially located cylindrical ice surfaces.



Main operating parameter

$$\Gamma_v = \frac{G}{2 * \Pi} \left( \frac{m^2}{s} \right)$$

$G$  – flow rate ( $\frac{m^3}{s}$ )

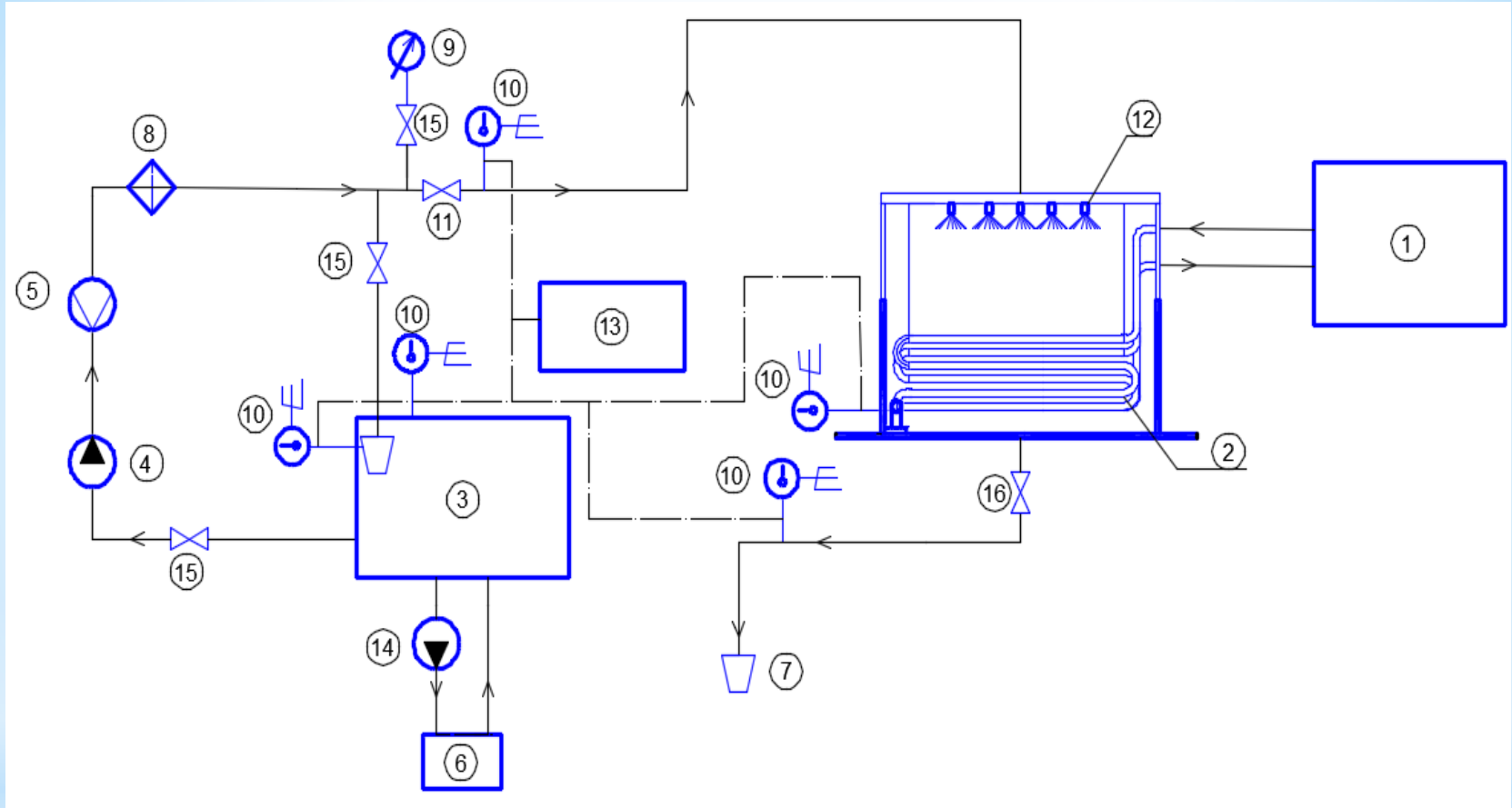
$\Pi$  – linear perimeter m

Thermal balance for a cooled fluid flow

$$\frac{m_{Bi} * Cp_i * (t_{ini} - t_{out_i})}{\Delta\tau} = \frac{r * m_{mi} + m_{mi} * Cp_i * (t_{out_i} - t_0)}{\Delta\tau}$$

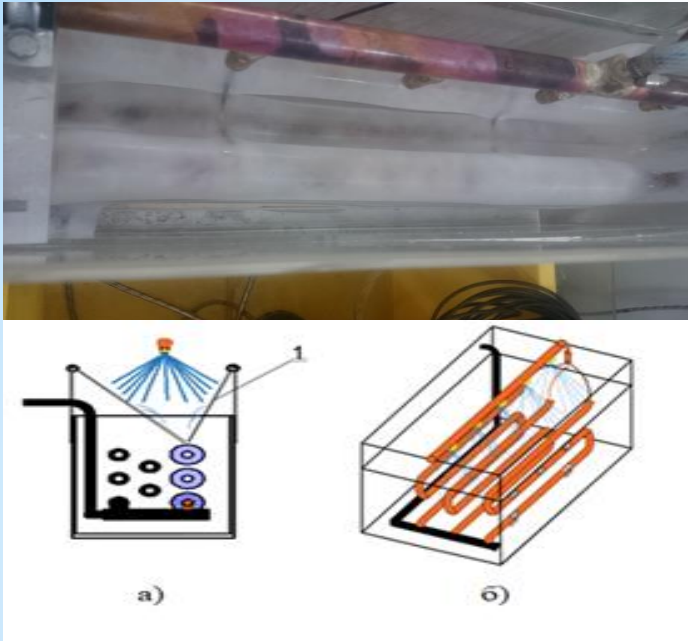
Sketch of a film coaxial ice bank

## 5. Scheme of the experimental stand



Scheme of the experimental stand: 1 - Compressor-condensing unit, 2 - Ice bank, 3 - Storage tank, 4 - Pump with frequency changer, 5 – Mass flow meter, 6 - Heater, 7 - Measuring tank, 8 - Filter, 9 - Manometer, 10 - Electronic thermometer, 11 - Regulating valve, 12 - Nozzles, 13 – Data recorder, 14 - Submersible pump, 15 – Shut-off valve, 16 - Flush valve

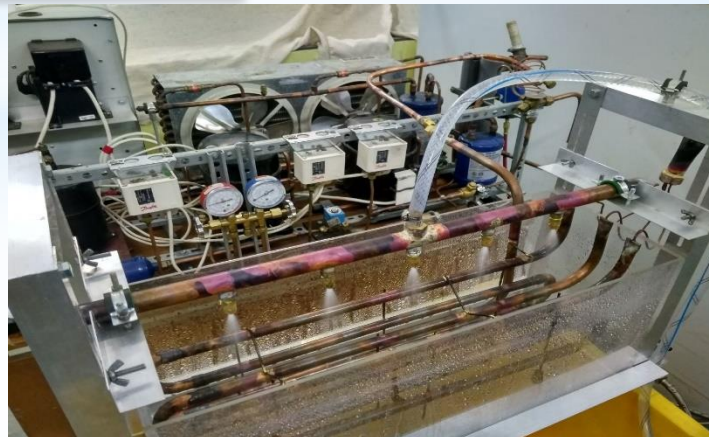
## 6. Experimental stand



Film heat exchanger with flat coils (PTA): a) water distribution during irrigation of one section; b) a three-section heat exchanger with water supply through nozzles: pos. 1 - slotted water distributor

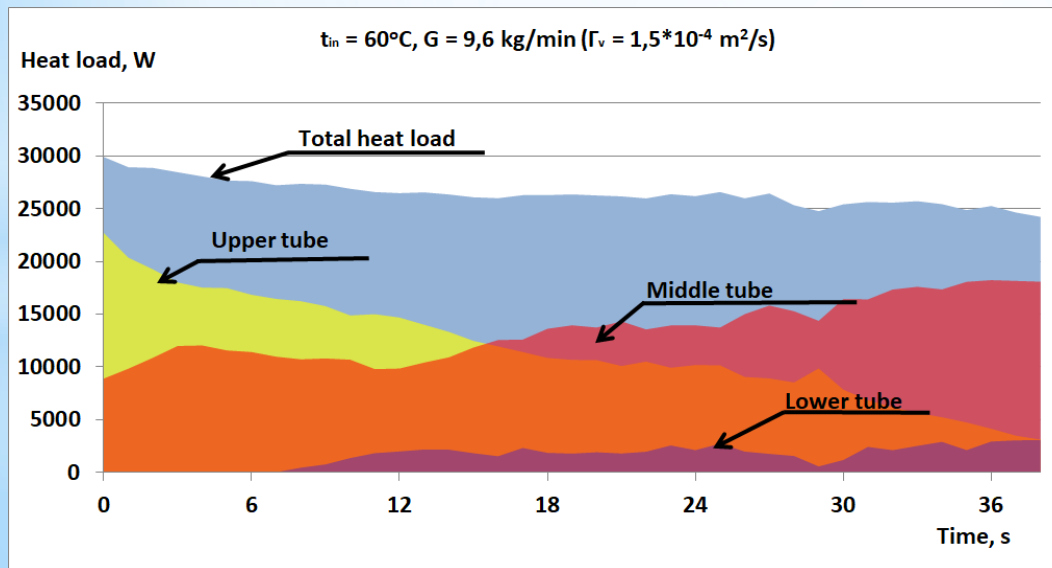
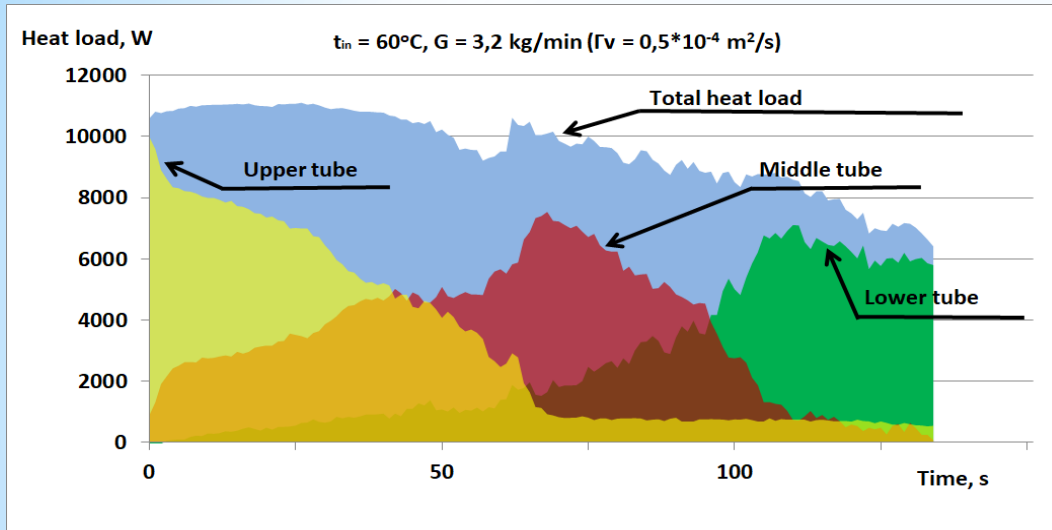
Coaxial film heat exchanger

It is necessary to determine:  
- Discharged heat Load  $Q$   
- Heat transfer coefficient  $\alpha$



The study was carried out with the financial support of the Russian Foundation for Basic Research within the framework of scientific project No. 20-08-00120

# 7. Discharged heat load



Range of change of operating parameters

Parameter	Regulation range
Water inlet temperature	from 20 °C to 60°C
Flow rate of water	from 3,2 kg/min to 9,6 kg/min
Density of irrigation	from $0,5 \cdot 10^{-4} \text{ m}^2/\text{s}$ to $1,5 \cdot 10^{-4} \text{ m}^2/\text{s}$

Specific heat load [ $\text{kW}/\text{m}^2$ ]

Comparative characteristics

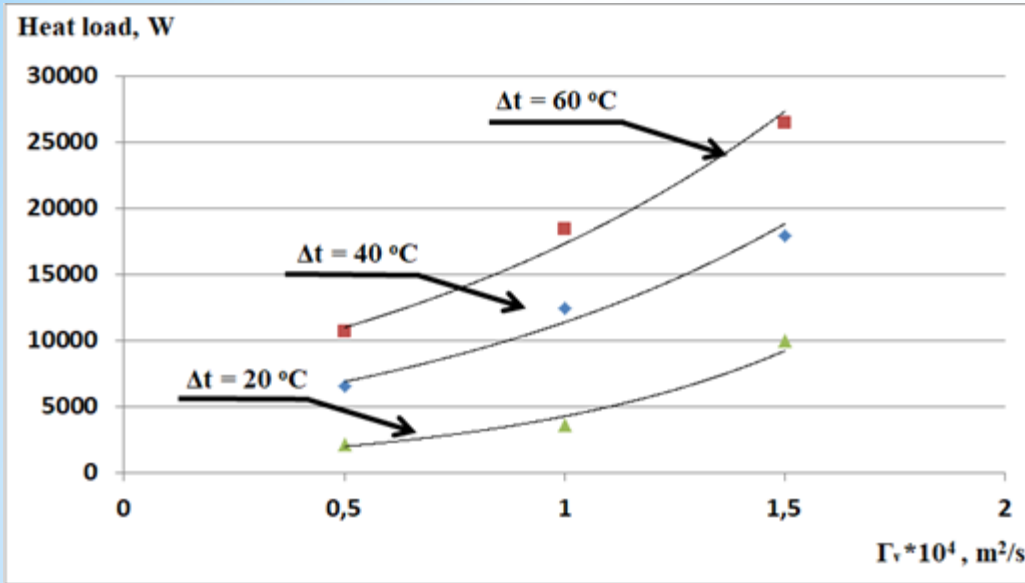
Plate heat exchangers :  
from 12 to 65  $\text{kW}/\text{m}^2$

Film heat exchanger  
(FHE):  
from 120 to 320  $\text{kW}/\text{m}^2$

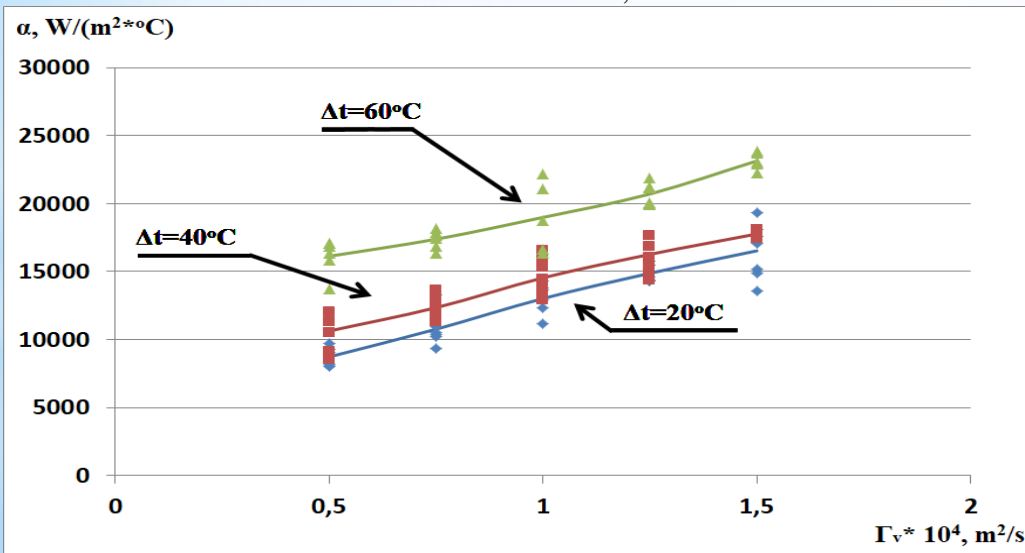
Diagrams of heat load distribution between pipes of one FHE section  $S=0,078 \text{ m}^2$ .



# 8. Efficiency of heat transfer



The graph of the dependency of the heat load removed by one section of the FHE with a surface  $S=0,078 m^2$



Dependency of the heat transfer coefficient on the density of irrigation

Newton-Richman law

$$q = \alpha(t_{liq} - t_s) \frac{W}{m^2}$$

$\alpha$  – proportion coefficient

$$\alpha = f(Re, \Delta t)$$

$$F_{ice} = var \rightarrow F_{FHE}$$

$$\alpha = \frac{Q_i}{(t_{liq} - t_{ice})F_{FHE}}$$

## 9. Conclusion

The advantage of the film ice bank has been experimentally proven with respect to the volumetric ice bank:

- the ability to cool water from a temperature of 60 ° C to 1 ° C in one pass;
- an experimental dependency of the heat transfer coefficient for a film ice bank on the irrigation density has been obtained.

In the investigated range, the values of the heat transfer coefficient are  $\sim 22000$  W/(m<sup>2</sup>\*°C) reduced to the surface of the heat exchanger and  $\sim 7000$  W/(m<sup>2</sup>\*°C) in relation to the melting surface, and in ice banks with volumetric melting do not exceed 300 - 500 W/(m<sup>2</sup>\*°C).

Specific heat load of FHE reaches 320 000 W/m<sup>2</sup>, significantly exceeding the same value for plate heat exchangers, which, according to open sources is from 12 000 to 65 000 W/m<sup>2</sup>

Fields of application:

- Dairy industry
- Brewing industry
- Air conditioning
- Emergency and abnormal surges in thermal load
- Cooling of systems with a pulsed heat sources (cooling of lasers, etc.)

*Thank you for your attention!*

# Additional materials



*Use of the natural cold of outside air*